

AERODYNAMIC CALCULATION OF THE MOVEMENT OF RAW COTTON BY A DRYING-TRANSPORT DEVICE

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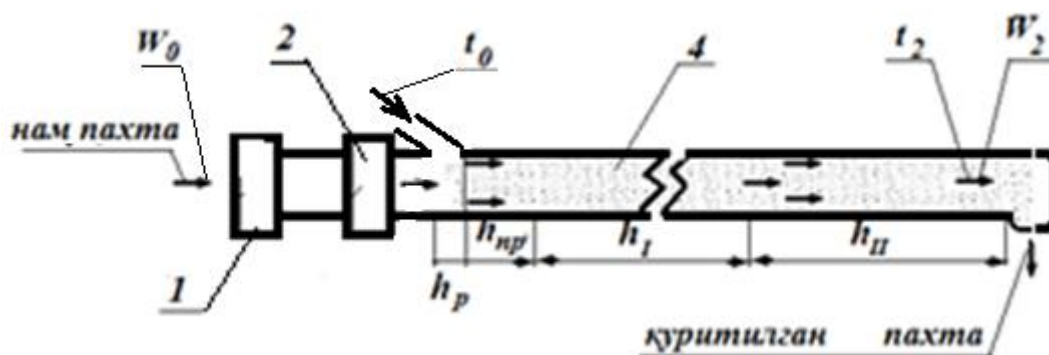
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ABSTRACT

This article studied the aerodynamic calculations of raw cotton moving in a stream of hot air in a drying and transport device, including the drying period depending on the speed of cotton in the pipeline, parameters such as the minimum temperature of the drying agent and its speed .

Keywords: solar collector, drying agent, raw cotton moisture, raw cotton movement, hot air flow, drying cycles, gravity, dynamic force, cotton lobule density, medium density, flow rate, flow regime, cotton lobule drag coefficient.

The principle of operation of the proposed drying and transportation device for drying cotton raw materials is based on the fact that wet cotton raw materials move along with the heated air flow. the economic scheme of the cotton drying and transportation device is shown.



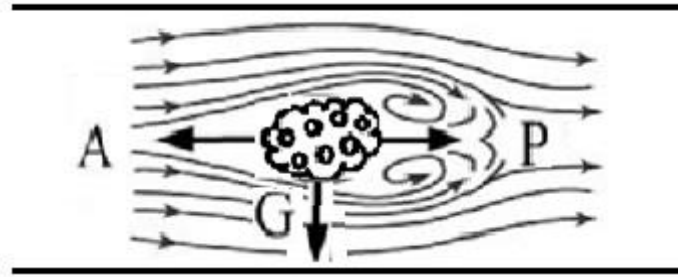
Picture.1. Kuritish - tashish kurilmazining calculation scheme.

1-colorifier; 2-fan; 3-supplying; 4-kuritish-tashish-kuvuri; h_r -accelerated survey of the site; h_{pr} -kuzish plot; h_I -kuritishning round rice; h_{II} -kuritishning round dish; t_o -heat transfer; t_o -mining; t_2 -mining; W_o -raw cotton sleeve.; w_o -cotton hand; w_2 -cotton gomashesin suspension namliga Нам пахта хом ашёси пневмокуритгичга таъминлагич орқали узатилади, ва у колорифердан the incoming hot air will mix with 90-100o C, continue its movement inside the drying and transportation pipeline, the length of the pipes is 150-250 meters, and a certain amount of moisture will be released from cotton raw materials along the length of the pipe.

The calculation of the aerodynamics of the drying and transportation device is based on determining the speed of movement of cotton raw materials, and below we will consider this issue.

The action of the dryer-carrier on a piece of cotton directed along the axis of the pipe in a stream of hot air: pain or gravity G , lifting (Archimedes) Force A , and dynamic pressure Force P of the flow assuming

that under the influence of forces, cotton raw materials act between the pipe, we cannot take into account the mutual friction force (Figure 2).



Picture. 2. Cotton homashesiga kuvur ichidagi Issyk introduced an ongoing movement to influence the kuchlar scheme.

Cotton buzlagini ellipsimon and uning the equivalent of the adjective d_x -cotton bravlagining diameter deb karasak, on hold:

$$G = \frac{\pi \cdot d_i^3}{6} * \rho_i * g;$$

$$A = \frac{\pi \cdot d_x^3}{6} * \rho_x * g;$$

$$P = \xi_{sud} * \frac{\pi \cdot d_i^2}{6} * \frac{V_{sud}^2 * \rho_x}{2};$$

Here ρ_x , - density of a piece of cotton; ρ_m -muxit density, кг/м^3 ; V_{sud} - flow rate, м/с ; ξ_{sud} - the coefficient of resistance of a piece of cotton, which depends on the mode of flow;

If $G > P$ or $G < P$, the cotton lump will act in a turbulent flow inside the pipe, if $G = P$ - , all forces acting on the cotton lump are balanced, the cotton lump will crawl at the bottom of the pipe, and it will be possible to say "creep" this speed. A piece of cotton with a speed equal to zero at the beginning of the pipe is captured by a stream of hot air, increasing their speed to a stable speed of movement.

And this is the accelerator part (h_p) the so-called. At the end of the accelerator section, the cotton splinter will have a speed determined based on the condition of the equality of gravity and the resistance of the medium.

At the end of the accelerator section (h_r), the cotton lump will have a speed of the following equality, which is determined from the balance of the force of the fan gravity and the Resistance Forces:

$$\frac{\pi \cdot d_x^3}{6} * (\rho_i - \rho_x) * g = \xi_{sud} * \frac{\pi \cdot d_i^2}{4} * \frac{V_{sud}^2 * \rho_x}{2}; \quad (1)$$

(1) from the equation, the creep rate of a piece of cotton will be equal to:

$$(2) \quad V_{sud} = \sqrt{\frac{4 * G * (\rho_i - \rho_x) * d}{3 * \rho_x * \xi_{sud}}}$$

The task of thermal calculation of the drying and transportation device is to determine the diameter and length of the drying pipe. Below is a simplified method of thermal calculation of the drying and transportation device [1].

Heat consumption for drying cotton raw materials: the heat consumption for heating wet cotton raw materials consists of the sum of the heat consumption in the I - period of drying and the heat consumption in the II-drying period:

$$Q_c = Q_{np} + Q_I + Q_{II}.$$

The initial heating period for a piece of cotton is equal to:

$$Q_{np} = G_{gur} * (C_m + C_v * t_2) * (W_m - W_o).$$

The heat consumption during the first drying (I) period is determined by the following formula:

$$Q_I = G_{qur} * (W_o - W_k) * r_1$$

For heat consumption during the second drying (II) period:

$$Q_{II} = G_{qur} * [(C_m + C_V * W_2) * (t_2 - t_m) + (W_k - W_2) * r_2],$$

In this case, G_{qur} is a mass of hot air spent on dry cotton raw materials,

C_m, C_V, C_{II} - heat capacity of absolute dry cotton, W_o, W_k, W_k - initial, critical and final moisture content of cotton raw materials, t_o, t_2, t_m - initial, critical and final tribute of cotton raw materials, r_1, r_2 - evaporation of moisture during the I and II period of drying.

Loss of heat to an external fan:

$$Q_{Таш} = k * F_{пп} * \Delta t \approx 0,1 * Q_c.$$

Total consumption of drying agent:

$$Q_a = \frac{Q_n + Q_{tash}}{c_r * (t_{r1} - t_{r2})},$$

Here c_r - average heat capacity of the drying agent, t_{r1}, t_{r2} - the Charter of the drying agent at the entrance and exit to the drying chamber.

Depending on the consumption of the drying agent, the size surface and diameter of the drying device pipe are calculated

$$F_{quv} = \frac{L_a}{3600 * \rho_x * V_r},$$

$$D_{quv} = \sqrt{\frac{4 * F_{quv}}{\pi}},$$

in this $V_r = V_{БИТ} + (18 - 20 \text{ м/с})$ - the speed of the drying agent. The amount of heat supplied from the drying device to the cotton raw materials is determined by the heat exchange equation:

$$Q_t = \alpha * F_m * \Delta t = \alpha_V * F_{quv} * \Delta t = \alpha_V * F_{quv} * h_{quv} * \Delta t = \alpha_h * h_{quv} * \Delta t.$$

In the heat transfer equation F_m surface area of cotton flakes F_{quv} it is replaced by the cross-sectional area of its pipe. α_V - the concept of the amount of heat transferred to cotton raw materials per unit of time, α_V volume heat transfer coefficient was introduced -

1 м^3 the amount of heat that the pipe transfers to the raw material of wet cotton in T khajm. The volume of the heat exchange coefficient will be in the range of 100-1200 $\text{W}/(\text{м} * \text{K})$.

The volume of the coefficient of heat exchange is determined by the following tengama: $\alpha_V = \alpha * f_{ud}$

in this $f_{ud} = \frac{F_m}{V_{quv}} = 6 * \beta_V / (d_m * \rho_m)$ - relative surface of heat exchange m^2/m^3 ;

V_{quv} - volume of pipe occupied by cotton raw materials, m^3 ;

$\beta_V = \frac{G_{qur}}{V_r} * F_{quv}$ - the amount of available cotton raw materials in the pipe, kg/m^3 .

The heat exchange surface (the surface of the cotton lump) is calculated as follows: $F_m = \pi * d_i^2 * n = 6 * G_{qur} / (d_m * \rho_m)$,

In this $n = \frac{G_{qur}}{V_m * \rho_m} = 6 * G_{qur} / (\pi * d_m^3 * \rho_m)$ - the number of pieces of cotton raw materials inside the pipe.

Drying-finding the length of the carrying pipe, drying will consist of the sum of periods:

$$H_{quv} = \frac{Q_n - Q_{tash}}{3,6 * \alpha_V * F_{quv} * \Delta t},$$

The convective heat exchange coefficient for creeping cotton lumps in the pipe is calculated as follows:

$$\alpha = 2 * \lambda_r / d_m \quad \text{учун} \quad Re_{sud} < 20$$

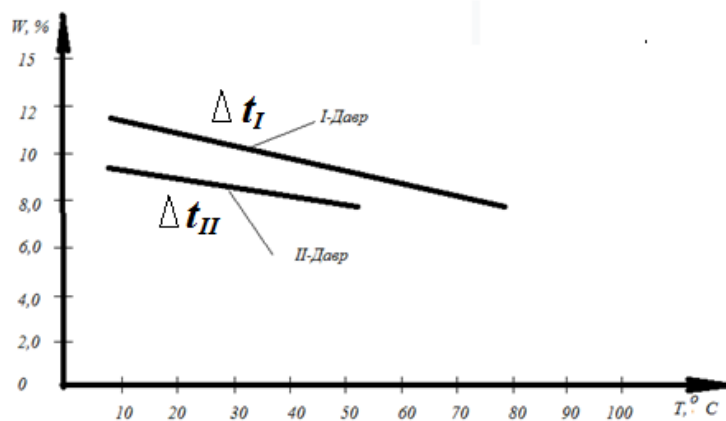
$$\text{ёки: } \alpha = 0,186 * Re_{sud}^{0,8} * \lambda_r / d_m \quad \text{учун} \quad 20 < Re_{sud} < 480$$

$$\text{ёки: } \alpha = 1,14 * Re_{sud}^{0,8} * \lambda_r / d_m \quad \text{учун} \quad 480 < Re_{sud} < 2000$$

For drying cotton raw materials, the waste stream is treated for each drying period:

$$\Delta t_I = \frac{(t_1 - W_1) - (t_2 - W_2)}{\ln \frac{(t_1 - W_1)}{(t_2 - W_2)}} = \frac{(90 - 12) - (40 - 8)}{\ln \frac{(90 - 12)}{(40 - 8)}} = \frac{78 - 32}{\ln \frac{78}{32}} = \frac{46}{\ln 2,43} = \frac{46}{0,8909} = 51,63^\circ\text{C}$$

$$\Delta t_{II} = \frac{(70 - 10) - (40 - 8)}{\ln \frac{(70 - 10)}{(40 - 8)}} = \frac{28}{\ln \frac{60}{32}} = \frac{28}{\ln 1,875} = \frac{28}{0,628} = 44,5^\circ\text{C}$$



3.- picture. Drying of cotton raw materials-a graph of the connection of the rate of acting cotton raw materials in the transport device to the minimum Charter of the drying agent for the 1st and 2nd period of drying

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